## APPENDIX I:

## CLAIM AMENDMENTS:

Amend Claims 1 to 9, 12 and 13 as indicated in the following listing of the claims:

- 1. (currently amended) An apparatus suitable for producing shaped bodies comprising thermoplastic polymers from monomers which form such polymers in a batch process, comprising
  - a) at least one reactor suitable for the batchwise preparation of a melt of a thermoplastic polymer from monomers which form such a polymer,
  - b) a piping system which comprises at least one pipe which forms a circuit and which is suitable as circulation line for the melt of the thermoplastic polymer and
  - c) at least one apparatus suitable for the production of shaped bodies from the melt of a the thermoplastic polymer,

## wherein

the <u>at least one</u> reactor  $\frac{1}{1}$  reactors a) is  $\frac{1}{1}$  connected to the piping system b) and

the <u>at least one</u> apparatus <del>or apparatuses</del> c) is<del>/are</del> connected to the piping system b).

- 2. (currently amended) An apparatus as claimed in claim 1, wherein the at least one reactor or reactors used in a) is/are suitable for a the reaction at a pressure in the range from 0 to 3 MPa and at a temperature in the range from 100 to 380 C 300°C.
- 3. (currently amended) An apparatus as claimed in claim 1, wherein the piping system b) additionally has a conveying device suitable for moving the melt of the thermoplastic polymer in <u>a</u> the longitudinal direction of the piping system.
- 4. (currently amended) An apparatus as claimed in claim 1, wherein at least one apparatus c) is a granulator—is used as apparatus c).
- 5. (currently amended) An apparatus as claimed in claim 1, wherein at least one apparatus c) is a spinning apparatus—is used as apparatus c).

- 6. (currently amended) An apparatus as claimed in claim 1, wherein at least one apparatus c) is an apparatus for producing a film is used as apparatus c).
- 7. (currently amended) An apparatus as claimed in claim 1, wherein the the piping system b) comprises
  - a first section which is adapted to allow the melt to flow from the direction of the at least one reactor a) in the direction of the at least one apparatus c), and
  - a second section which is adapted to allow the melt to flow from the direction of the at least one apparatus c) in the direction of the at least one reactor a),

## and wherein

the <u>first section of the piping system b) has a</u> mean average pipe diameter in the <u>piping system b)</u> between the <u>first reactor a)</u> and the <u>last apparatus c)</u> viewed in the flow direction <u>which</u> is equal to or greater than the mean average pipe diameter between the <u>last apparatus c)</u> and the <u>first reactor a)</u> viewed in the flow direction <u>in the</u> second section.

- 8. (currently amended) An apparatus as claimed in claim ± 7, wherein the ratio of the mean average pipe diameter in the first section piping system b) between the first reactor a) and the last apparatus c) viewed in the flow direction to and the mean average pipe diameter in the second section between the last apparatus c) and the first reactor a) viewed in the flow direction is in the range have a ratio of from 1:1 to 10:1.
- 9. (currently amended) An apparatus A process for producing shaped bodies comprising thermoplastic polymers from monomers which form such polymers in a batch process in an apparatus as claimed in claim 1, which comprises
  - a) preparing a melt of a thermoplastic polymer batchwise from monomers which form such a polymer in at least one reactor,
  - b) feeding the melt of the thermoplastic polymer obtained in step a) into a piping system which comprises at least one pipe which forms a circuit and which is suitable as circulation line for the melt of the thermoplastic polymer, and moving it the melt through the piping system at a mean average wall shear rate in the range from 0.1 to 100 s<sup>-1</sup> and a mean average flow velocity in the range from 0.1 to 100 cm/s,

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- c) taking the melt of the thermoplastic polymer from the piping system b) and producing shaped bodies from the thermoplastic polymer.
- 10. (original) A process as claimed in claim 9, wherein monomers selected from the group consisting of adipic acid, hexamethylenediamine, terephthalic acid, xylylenediamine, hexamethylenediammonium adipate, caprolactam and mixtures thereof are used in step a).
- 11. (original) A process as claimed in claim 9, wherein hexamethylene-diammonium adipate is used as monomer in step a).
- 12. (currently amended) A process as claimed in claim 9, wherein the temperature of the melt of the thermoplastic polymer in the piping system used in step b) is from 0 to 60°C 60\_C above the melting point of the thermoplastic polymer determined in accordance with ISO 11357-1 and 11357-3.
- 13. (currently amended) A process as claimed in claim  $\pm 9$ , wherein, in step c), melt of the thermoplastic polymer is taken continuously from the piping system.

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